

Potential-Induced Synthesis and Structural Identification of Oxide-Derived Cu Electrocatalysts for Selective Nitrate Reduction to Ammonia

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ABSTRACT: Developing effective electrocatalysts for nitrate reduction to ammonia is paramount for ammonia synthesis while addressing the water pollutant issue. Identifying the active structure and its correlation with catalytic behavior during the reaction process is essential and challenging for the rational design of advanced electrocatalysts. Herein, starting from Cu_2O particles with controllable crystal facets, the electrochemically reconstituted Cu/ Cu_2O was fabricated as a suitable catalytic system, and the relationship between the chemical state of copper and product selectivity in the nitrate reduction reaction was studied. At -0.9 V versus reversible hydrogen electrode, the oxide-derived Cu^0 (OD-Cu) cube achieved a high ammonia Faradaic efficiency of 93.9% and productivity of up to $219.8 \mu\text{mol h}^{-1} \text{cm}^{-2}$, surpassing those of most Cu-based catalysts. In situ Raman analysis, well-designed pulsed electrolysis experiments, and theoretical calculations showed that ammonia was preferentially produced on OD-Cu at high reduction potentials and the presence of the Cu/ Cu_2O interface favored nitrite formation at low reduction potentials. The high ammonia selectivity of the OD-Cu cube originated from the enhanced adsorption of nitrate and lower reaction barrier of the potential-determining step ($^*\text{NH}_3 \rightarrow \text{NH}_3$). This work presents an effective strategy to boost electrocatalysis and offers an insight into the real active phase and corresponding catalytic behavior of Cu-based electrocatalysts.

KEYWORDS: nitrate reduction reaction, oxide-derived copper, ammonia synthesis, in situ Raman, electrochemical reconstruction



1. INTRODUCTION

Ammonia (NH_3), as an important commodity or energy carrier, is critical to chemical synthesis, fertilizer manufacturing, and renewable energy storage and conversion, greatly impacting the development of modern society.^{1–5} Current large-scale NH_3 synthesis still relies heavily on the energy- and capital-intensive Haber–Bosch process, which consumes 2% of the global energy and produces >1% of the global CO_2 emissions.^{6,7} Recently, intensive efforts have been devoted to developing a sustainable and eco-friendly alternative for NH_3 production, and the electrochemical nitrogen reduction reaction (NRR) under mild conditions powered by renewable energy sources has attracted extensive attention.^{8–11} However, the selectivity and yield of NH_3 produced via the NRR are extremely low because of the low water solubility and high $\text{N}\equiv\text{N}$ bond dissociation energy (945 kJ mol^{-1}) of N_2 , which are far behind the industrial requirements.^{12,13} The electroreduction of nitrate (NO_3^-), which has a high water solubility and low $\text{N}=\text{O}$ bond dissociation energy (204 kJ mol^{-1}),^{14,15} has great potential to produce NH_3 at a faster reaction rate while eliminating NO_3^- pollution in the environment.^{16–18} Nevertheless, the NO_3^- reduction reaction (NO_3RR) to NH_3 involves multiple electron and proton transfer processes, which

may afford different products including NO_2^- , NO , N_2 , and NH_2OH ,^{19–22} and thus exhibits an unsatisfactory NH_3 selectivity. Therefore, developing a highly efficient and selective catalyst for the NO_3RR to NH_3 is a prerequisite.

Among the various alternatives, Cu-based materials have been extensively studied owing to their large numbers of unpaired d-orbital electrons, moderate energy barriers for intermediate adsorption, and suppression of the hydrogen evolution reaction (HER).^{23–25} In recent years, various efficient Cu-based catalysts, such as defect-rich Cu(100),²⁶ $\text{CuBDC@Ti}_3\text{C}_2\text{T}_x$,²⁷ Cu@C ,²⁸ Rh@Cu NWs,²⁹ CuCoSP ,³⁰ and Cu-N-C ,³¹ have been reported in NO_3RR to NH_3 . Particularly, the oxide-derived Cu-based catalyst fabricated via in situ electrochemical reconstruction exhibited an enhanced selectivity of NH_3 during NO_3^- reduction.^{32–35} For example,

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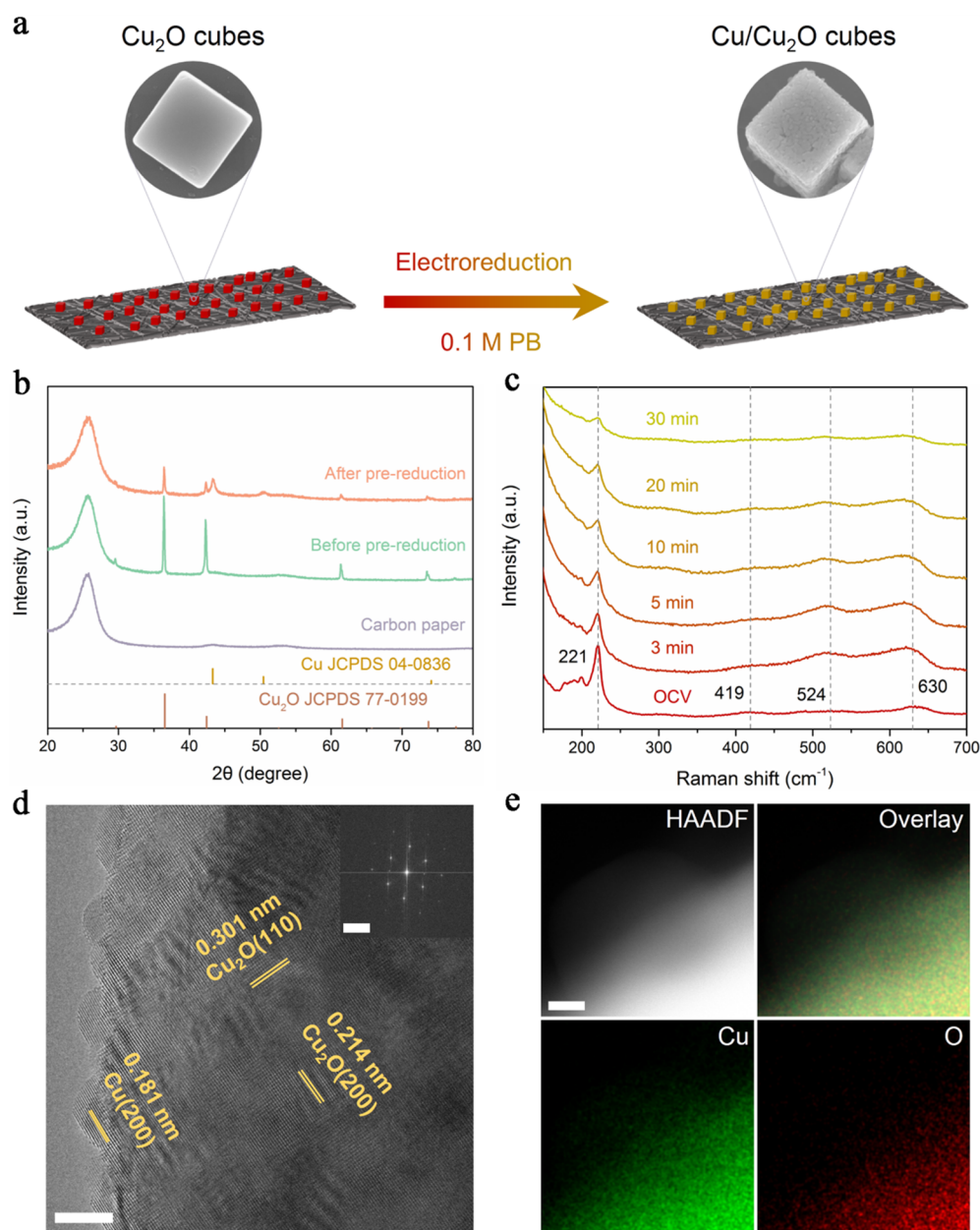


Figure 1. Structural characterization of Cu/Cu₂O interfaces. (a) Schematic illustration of the construction of the stable Cu/Cu₂O interface structure by electrochemical prereluction strategy at -0.6 V vs RHE in 0.1 M PB solution. (b) XRD patterns of Cu₂O cubes before and after prereluction stabilization. (c) In situ Raman spectra collected during the prereluction of Cu₂O cubes. (d) HRTEM characterization of the Cu/Cu₂O interface (inset: the FFT image). (e) STEM image and the corresponding elemental mapping of the distribution for Cu (green) and O (red) at the Cu/Cu₂O interface. Scale bars: 5 nm (d), 5 nm (e), and 5 $1/\text{nm}$ for inset in (d).

Zhang's group constructed a Cu/Cu₂O interface as the active phase by in situ reduction of CuO arrays and achieved highly selective NO₃[−] reduction to NH₃.³⁶ Similarly, Ren et al. reported that the thin outer concave-convex oxide layer of the Cu/Cu₂₊₁O interface structure possessed an optimized Cu d-band center and adsorption energies of key intermediates and afforded high catalytic performance.³⁷ These studies suggest that the improved NH₃ selectivity of the Cu/Cu₂O interface is associated with a reduced energy barrier for NO₃[−] reduction to NH₃ on Cu⁺ active sites.^{19,38} However, the unstable Cu²⁺/Cu⁺ species are in situ electrochemically transferred to Cu⁰ during the NO₃[−] reduction process, which is claimed as an intrinsically active site.^{26,39} Despite these achievements, the real catalytic structure and its relationship with the activity/

selectivity of these Cu-based materials remain in disagreement. Monitoring the dynamic structural changes and the corresponding effects on the activity of Cu-based catalysts during the NO₃RR process, such as the oxidation state of Cu, is necessary to develop new advanced electrocatalysts for NO₃[−] reduction to NH₃. However, because Cu-based materials are susceptible to oxidation/reduction under working conditions and probing limitations, understanding the true active site and its correlation with the catalytic performance under the realistic working condition is full of challenges.^{40,41} In this context, it is necessary to construct a suitable model catalyst system and utilize the advanced in situ characterization.

Herein, starting from Cu₂O particles with controllable crystal facets, a suitable Cu/Cu₂O model catalyst was

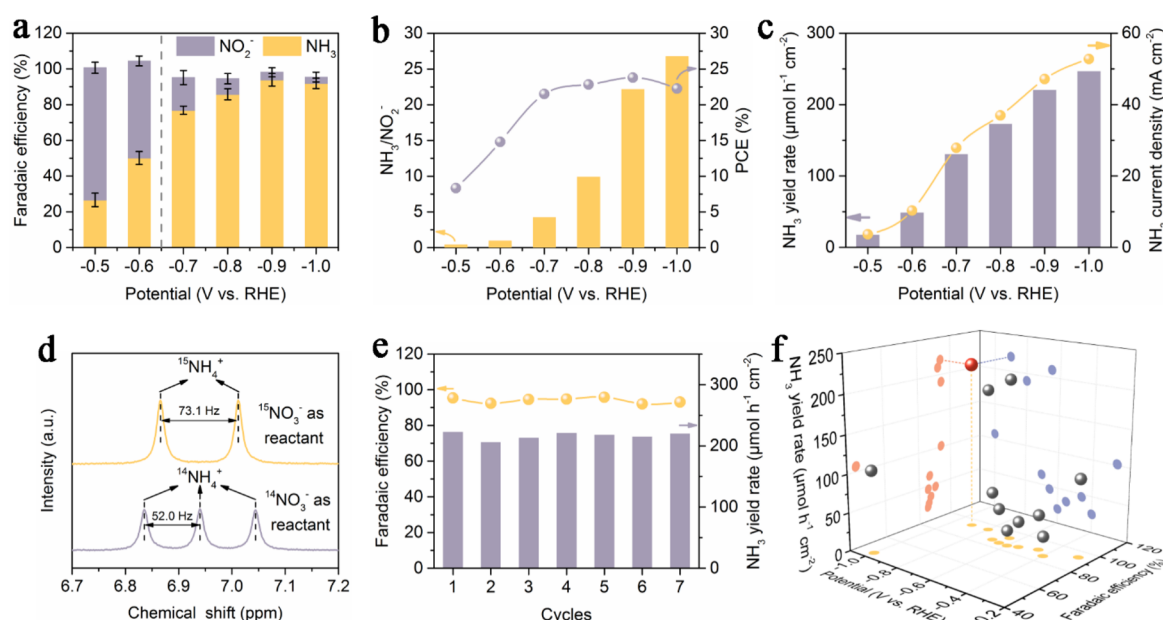


Figure 2. Electrochemical NO_3RR performance of *c*-Cu/Cu₂O in 0.1 M PB solution containing 0.1 M KNO₃. (a) Faradaic efficiencies of NH₃ and NO₂[−] at different potentials. (b) Faradaic efficiency ratio of NH₃ to NO₂[−] and cathode power conversion efficiency (PCE) at different potentials. (c) The corresponding NH₃ production rate and partial current density at different potentials. (d) ¹H NMR spectra of ¹⁴NH₄⁺ and ¹⁵NH₄⁺ produced after NO₃RR using ¹⁵NO₃[−] and ¹⁴NO₃[−] as reactants, respectively. (e) Cycling stability measurements of *c*-Cu/Cu₂O at −0.9 V vs RHE. (f) Performance comparison of different reported Cu-based catalysts for NO₃[−] electroreduction to NH₃ in neutral electrolyte (See detailed information in Table S1). Red ball represents the performance of this work. The error bars represent the standard deviation of three independent samples.

fabricated via an electrochemical prereluction method, and the structural evolution of Cu-based catalysts during the NO₃RR at different potentials was systematically investigated. The effect of the chemical state of Cu on the product selectivity of the NO₃RR was verified utilizing a rational electrochemical strategy combined with in situ Raman spectroscopy and theoretical calculations. Results show that the Cu/Cu₂O interface formed at low reduction potentials (≥ -0.6 V vs reversible hydrogen electrode (RHE)) facilitates the conversion of NO₃[−] to NO₂[−]. By contrast, at high reduction potentials (< -0.6 V vs RHE), the in situ generated oxide-derived Cu⁰ (OD-Cu) is the genuine active phase for the highly selective NO₃[−] reduction to NH₃. The OD-Cu cube exhibits a maximum NH₃ Faradaic efficiency (FE) of 93.9% and a productivity of 219.8 $\mu\text{mol h}^{-1} \text{cm}^{-2}$ at −0.9 V vs RHE. ¹⁵N isotope-labeling experiments confirm that the detected NH₃ originates from the NO₃RR. In situ infrared (IR) spectroscopy analysis and density functional theory (DFT) calculations show that the improved NH₃ selectivity on OD-Cu is because of the enhanced adsorption of NO₃[−], the promoted formation of key intermediate *NOH, and the inhibited competitive HER. Our results provide a comprehensive fundamental understanding on the nature of the active sites for the selective NO₃RR on Cu-based electrocatalysts and will guide the rational optimization of efficient electrocatalysts for NH₃ production.

2. RESULTS AND DISCUSSION

Cu₂O cubes, referred to as *c*-Cu₂O, were synthesized by a modified method,⁴² as proven using scanning electron microscopy (SEM), transmission electron microscopy (TEM), X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), and Raman results (Figures S1–S5). Notably,

a neutral phosphate buffer (PB) solution was used as the electrolyte in the electrochemical reduction method because it could inhibit the competitive HER.^{43,44} Therefore, first, the *c*-Cu₂O precursors were drop-coated on carbon paper; then, electrochemical prereluction reconstruction was performed at a bias potential of −0.6 V vs RHE in a 0.1 M PB solution (pH = 7) until a stable current was achieved (Figures 1a and S6). XRD results of the *c*-Cu₂O precursors display two characteristic peaks at 36.5° and 42.4°, attributed to the (111) and (200) facets of Cu₂O (JCPDS 77-0199; Figure 1b), respectively. These characteristic peaks of Cu₂O are still observed in the XRD spectra after prereluction stabilization along with a new set of peaks corresponding to metallic Cu (JCPDS 04-0836), suggesting the presence of a relatively stable bulk structure of the synthesized Cu₂O precursor with only partial reduction of Cu₂O to metallic Cu. SEM images clearly show that the Cu-based catalysts inherit the original bulk structure of the Cu₂O precursors but exhibit an increased surface roughness after prereluction (Figure S7), improving the electrochemically active surface area (ECSA) and exposing more reaction sites (Figure S8).

In situ Raman spectroscopy was further performed in a commercial H-type Raman cell to monitor the dynamic phase evolution during the prereluction of Cu₂O (Figures 1c and S9). The characteristic Raman modes of Cu₂O (221, 419, 524, and 630 cm^{−1}) are preserved but exhibit a weakened intensity after the prereluction process, implying that the Cu₂O precursor is not completely reduced. The coexistence of Cu and Cu₂O structures was obtained using this prereluction approach. To further illustrate the structure and composition of Cu₂O after prereluction, high-resolution transmission electron microscopy (HRTEM) of the edge region for *c*-Cu₂O was performed immediately after prereluction (Figure 1d). Only superficial Cu₂O was reduced to Cu particles

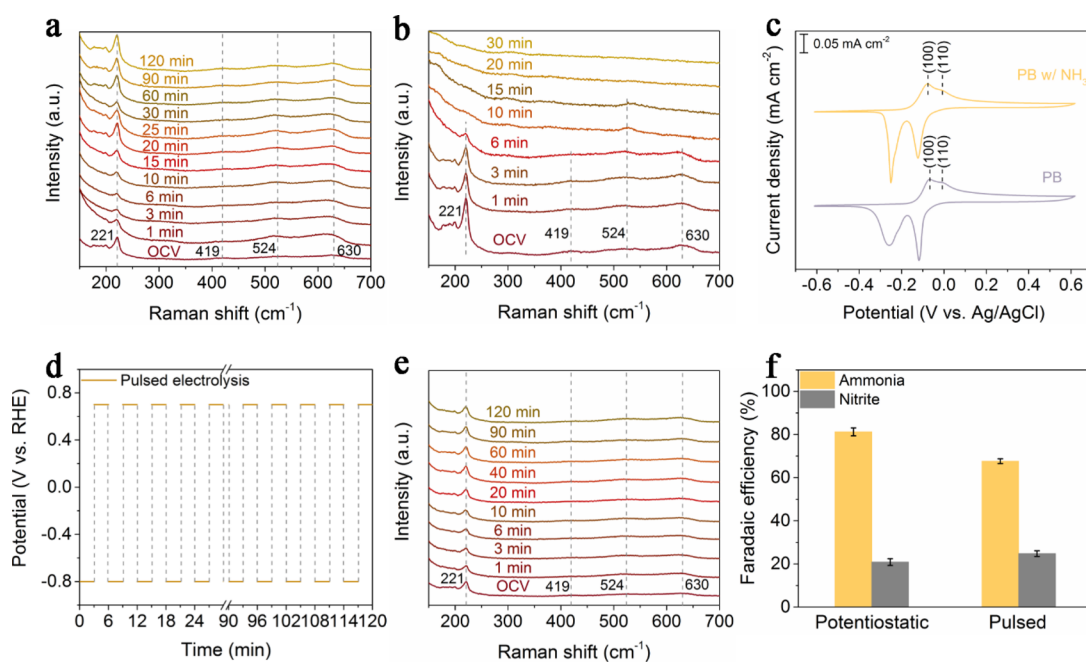


Figure 3. Pulsed electrolysis measurements. In situ Raman spectra of *c*-Cu/Cu₂O as a function of reaction time at (a) -0.6 and (b) -0.9 V vs RHE, respectively. (c) CV curves of OD-Cu-c in 0.1 M PB electrolyte with and without 0.01 M ammonia. The scan rate is 1 mV s⁻¹. (d) Periodic reduction and oxidation of *c*-Cu/Cu₂O under NO₃⁻ pulsed electrolysis at $E_{ca} = -0.8$ V and $E_{an} = 0.7$ V vs RHE. (e) In situ Raman spectra of *c*-Cu/Cu₂O as a function of reaction time under pulsed electrolysis. (f) Comparison of Faradaic efficiencies of NH₃ and NO₂⁻ for *c*-Cu/Cu₂O under different electrolysis conditions.

belonging to the (200) planes, while the bulk phase was relatively stable, as indicated by the observed single-crystal nature in the fast Fourier transform (FFT) pattern (inset in Figure 1d). Scanning transmission electron microscopy-energy dispersive X-ray spectroscopy (STEM-EDS, Figure 1e and Figure S10) images show that the surface and bulk of *c*-Cu₂O have different Cu and O atomic contents after prerduction, unlike the initial *c*-Cu₂O, which has a uniform distribution of Cu and O elements (Figure S11). The atomic contents of the bulk phase are similar to those of *c*-Cu₂O before prerduction, and only Cu atoms are detected on the surface, further confirming the uniform spatial distribution of metallic Cu nanoparticles on the surface. Therefore, a Cu/Cu₂O interface structure is successfully formed from *c*-Cu₂O via the prerduction method, which is used as a model electrocatalyst for the subsequent NO₃RR. For convenience, the Cu/Cu₂O interface structure is hereafter denoted as *c*-Cu/Cu₂O.

The NO₃⁻ electroreduction performance of *c*-Cu/Cu₂O was assessed under ambient conditions in a standard three-electrode H-type electrolytic cell. Chronoamperometry tests were performed in a 0.1 M PB electrolyte containing 0.1 M KNO₃ over a potential ranging from -0.5 to -1.0 V vs RHE for 2 h. Indophenol blue spectrophotometry and ¹H NMR spectroscopy were used to determine the concentration of NH₃, and the possible byproduct NO₂⁻ was quantified via ion chromatography (Figures S12–S14). To assess the selectivity of specific products, the potential-dependent FEs of NH₃ and NO₂⁻ are shown in Figure 2a. When the applied potential is more positive than -0.6 V vs RHE, the predominant reduction product is NO₂⁻, whereas NH₃ is the main product when the applied potential is more negative than -0.6 V vs RHE. Specifically, at -0.9 V vs RHE, *c*-Cu/Cu₂O exhibits a maximum NH₃ FE of 93.9%. Notably, the sum of the FEs for reduction products NH₃ and NO₂⁻ is approximately 100%

over the entire applied potential range, suggesting that the NO₃RR can effectively inhibit the HER. Additionally, the NH₃ and NO₂⁻ ratios of the *c*-Cu/Cu₂O catalyst were compared (Figure 2b). At -0.9 V vs RHE, the *c*-Cu/Cu₂O catalyst exhibits the highest NH₃ to NO₂⁻ ratio of 22.1, further indicating that *c*-Cu/Cu₂O preferentially produces NH₃ rather than NO₂⁻ at high cathodic potentials. Furthermore, the half-cell power conversion efficiency (PCE) of *c*-Cu/Cu₂O for NH₃ is 23.8% at -0.9 V vs RHE. The yield rate (Y_{NH_3}) and partial current density (J_{NH_3}) of NH₃ increase with an increase in cathodic potential (Figure 2c), consistent with previous reports.^{28,45} Impressively, *c*-Cu/Cu₂O exhibits an NH₃ yield rate and partial current density of up to 246.2 μmol h⁻¹ cm⁻² and 52.8 mA cm⁻² at -1.0 V vs RHE, respectively.

To verify that the generated NH₃ was from the NO₃RR instead of other nitrogenous pollutants, K¹⁵NO₃ was used as the starting nitrogen source in the ¹⁵N isotope-labeling experiments. As shown in the ¹H NMR spectra (Figure 2d), when ¹⁴NO₃⁻ is used as the reactant for the electrolysis reaction, the ¹H NMR spectrum of the detected NH₄⁺ exhibits a typical three-peak feature with a coupling constant of 52.0 Hz, whereas when ¹⁴NO₃⁻ is replaced by ¹⁵NO₃⁻, the ¹H NMR spectrum of the detected ¹⁵NH₄⁺ exhibits a typical double-peak feature with a coupling constant of 73.1 Hz. The ¹⁵N isotope-labeling results strongly suggested that NH₃ detected in the electrolyte is indeed from the NO₃RR.⁴⁶ As determined using ¹H NMR spectroscopy, the corresponding FE and yield rate of *c*-Cu/Cu₂O for NH₃ production at -0.9 V vs RHE are 93.6% and 217.7 μmol h⁻¹ cm⁻², respectively, consistent with the UV–Vis spectra (Figure S15). No NH₃ is detected when blank PB solutions are used for electrolysis, confirming that NH₃ is produced only via the electroreduction of NO₃⁻. The durability of the *c*-Cu/Cu₂O catalyst was verified by performing continuous NO₃⁻ electrolysis at -0.9 V

vs RHE. As shown in Figure 2e, the NH_3 yield rate and FE remain stable over the seven consecutive rounds of the reaction, without an apparent trend of decay. When the electrolytes after electrolysis are stained with an indophenol blue indicator, they all show an almost identical color, again demonstrating the good catalytic stability of the Cu-based material (Figure S16).

The structure of the c-Cu/Cu₂O catalyst after NO_3^- reduction electrolysis at different potentials was characterized via ex situ XRD (Figure S17). The c-Cu/Cu₂O catalyst undergoes a phase transition as the cathodic potential increases from -0.5 to -1.0 V vs RHE. Specifically, the initial Cu/Cu₂O interface structure is reconstructed into the metallic state Cu when the reaction potential is more negative than -0.6 V vs RHE. However, the original cubic morphology of the c-Cu/Cu₂O catalyst is still preserved at operation potentials of -0.6 and -0.9 V vs RHE (Figure S18). The morphology and phase analyses of c-Cu/Cu₂O after the durability test at -0.9 V vs RHE further reveal that the initial Cu/Cu₂O mixed phase is reconstructed into the metallic state Cu⁰ without morphological damage (Figures S19 and S20). Therefore, the in situ generated OD-Cu is the true active phase during the first electrolysis and shows excellent stability for the subsequent selective NO_3^- electroreduction to NH_3 . Additionally, the NO_3RR performance of the oxide-derived Cu cube (abbreviated as OD-Cu-c) was compared with those of other recently reported Cu-based catalysts. Figure 2f and Table S1 show that OD-Cu-c has a superior NH_3 yield rate and FE for the electroreduction of NO_3^- to NH_3 in a neutral electrolyte than most other Cu-based materials.

To further investigate the effect of different oxidation states of copper on the NH_3 selectivity during NO_3^- reduction, the structural evolution of the c-Cu/Cu₂O catalysts under different applied potentials was monitored via in situ Raman spectroscopy. As depicted in Figure 3a, c-Cu/Cu₂O retains the characteristic Raman modes of Cu₂O (e.g., the $2\Gamma_{12}^-$ mode at 221 cm^{-1}) throughout the 2 h reaction when the applied potential is -0.6 V vs RHE.⁴⁷ However, when a negative potential of -0.9 V vs RHE is applied, the intensity of the Cu₂O peak gradually decreases and disappears within 15 min, indicating the complete reduction of the oxide to the metallic phase (Figure 3b). The results are consistent with the ex situ XRD characterization and further indicate that the oxide-derived metallic phase Cu⁰ is the true active phase for promoting the highly selective NH_3 synthesis from NO_3^- at -0.9 V vs RHE. To further confirm the universality of this conclusion, Cu₂O octahedron precursors (abbreviated as o-Cu₂O) were also synthesized, and the true active centers and their role in determining the selectivity of the NO_3^- reduction product were investigated using the same strategy (Figures S1–S7, S11, S17, S18, and S21–S24). The results showed that the potential-induced OD-Cu from the o-Cu₂O precursor is also the active phase for NH_3 production.

Additionally, linear sweep voltammetry (LSV) tests for NO_3^- reduction were performed on the OD-Cu-c catalyst in a 0.1 M PB solution with and without 0.1 M KNO_3 (Figure S25). Compared with the blank electrolyte, the increase in current density and positive shift of the onset potential of OD-Cu-c in PB solution containing 0.1 M KNO_3 indicate the catalytic activity for the NO_3RR . And the reduction peak at -0.4 V vs RHE is attributed to NH_3 generation.⁴⁸ Moreover, the LSV curves of OD-Cu-c highly overlap for five consecutive cycles, further verifying the excellent stability of the OD-Cu-c

catalyst. The advantages of the OD-Cu-c catalyst are further highlighted by performance comparison with commercial Cu microspheres (referred to as Cu MSs) with a similar particle size (Figure S26). The ECSA of different Cu-based samples was estimated using cyclic voltammetry (CV) measurements under a potential window without Faraday reactions at different scan rates (Figure S27). LSV curves showed that OD-Cu-c exhibits a larger current density than Cu MSs under the same test conditions (Figure S28). Moreover, the higher intrinsic NO_3RR activity of OD-Cu-c than Cu MSs can be further gleaned from the larger current density in the ECSA-normalized LSV curves. Potentiostatic electrocatalysis results show that the selectivity of NH_3 over OD-Cu-c is higher than that over Cu MSs in the potential ranging from -0.7 to -1.0 V vs RHE. For example, at -0.9 V vs RHE, OD-Cu-c and Cu MSs exhibit FEs of 93.88 and 81.69%, respectively. Furthermore, the turnover frequency (TOF) was calculated to evaluate the ability of the catalyst to convert the reactants into the desired products per catalytic site and per unit of time.⁴⁹ The TOFs of OD-Cu-c and Cu MSs for NH_3 production are 1.09×10^{-2} and $4.73 \times 10^{-3}\text{ s}^{-1}$ at -0.9 V vs RHE, respectively. These results suggest that the in situ formed Cu⁰ catalyst during the electrolysis process enables an efficient NO_3RR to NH_3 .⁴¹ The apparent activation energy (E_a) of different Cu-based samples for NO_3^- reduction to NH_3 was evaluated using their temperature-dependent performances and Arrhenius equation.⁴⁹ Figure S29 shows that the apparent activation energy of OD-Cu-c ($E_a = 11.3\text{ kJ mol}^{-1}$) is lower than that of Cu/Cu₂O ($E_a = 12.3\text{ kJ mol}^{-1}$) at a potential of -0.6 V vs RHE. At a potential of -0.9 V vs RHE, the E_a of OD-Cu-c is only 5.3 kJ mol^{-1} , which is one-third of that of Cu MSs ($E_a = 16.1\text{ kJ mol}^{-1}$). OD-Cu-c has a lower energy barrier than Cu/Cu₂O and Cu MSs for initiating electrocatalytic NO_3^- to NH_3 and thus exhibits a high intrinsic activity. The microstructures of OD-Cu-c and Cu MSs were characterized by HRTEM (Figure S30a–c). The results indicated that OD-Cu-c displays a Cu(100)-rich surface compared to Cu MSs dominated by Cu(111) facets, which was further confirmed by specific electrochemical adsorption voltammetry tests of OH^- on different facets of Cu (Figure S30d).^{26,50} Therefore, compared with Cu MSs, the high (100) surface fraction of OD-Cu-c might be responsible for its high intrinsic activity.

To study the effect of the oxidation state of Cu on the selectivity of NO_3^- reduction products, pulsed electrolysis^{51–53} was well-designed to modulate the chemical state composition of the c-Cu/Cu₂O catalyst through the periodic application of oxidative potential pulses over a short period. Before that, the electrochemical behavior of NH_3 oxidation over OD-Cu-c was first investigated (Figure 3c). Similar to the blank 0.1 M PB electrolyte, when the electrolyte comprises 0.1 M PB and 0.01 M NH_3 by the addition of concentrated NH_3 water (corresponding to the amount of NH_3 produced via NO_3RR), only two peaks ascribed to OH^- adsorption on the Cu(100) and Cu(110) surfaces are observed throughout the potential interval.²⁶ The absence of new oxidation peaks indicates that the Cu-based catalyst is inactive for electrocatalytic NH_3 oxidation. Therefore, pulsed electrolysis experiments were performed by periodically applying a reduction potential of -0.8 V vs RHE and an oxidation potential of 0.7 V vs RHE, respectively (Figure 3d). For comparison, potentiostatic electrolysis experiments of the NO_3RR at -0.8 V vs RHE were also performed (Figure S31). The structural evolution of the c-Cu/Cu₂O catalyst during pulsed electrolysis was

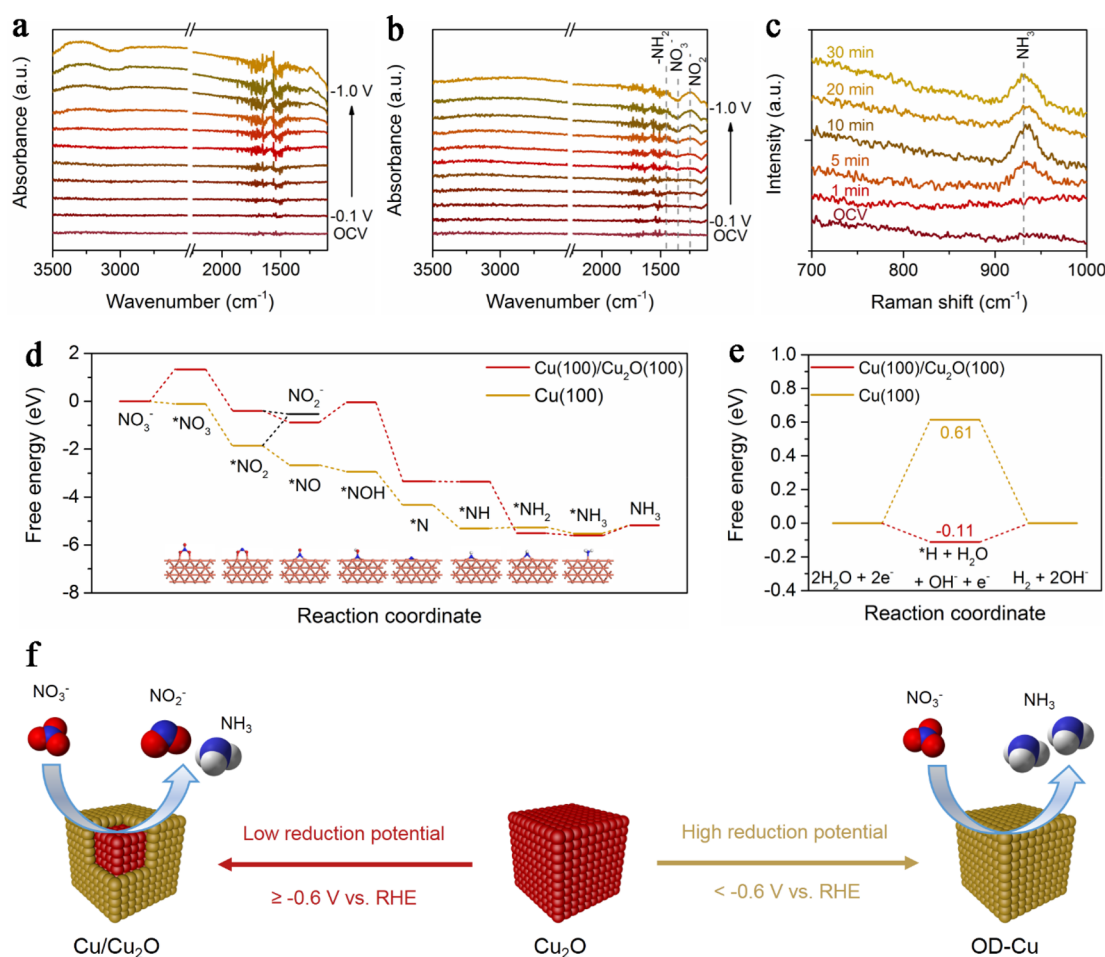


Figure 4. In situ spectroscopic characterization and theoretical calculations. (a) In situ ATR-FTIR spectra of OD-Cu-c acquired in 0.1 M PB solution. (b) In situ ATR-FTIR spectra of OD-Cu-c in 0.1 M PB solution containing 0.1 M KNO₃. (c) In situ Raman spectra of OD-Cu-c obtained under NO₃RR at -0.9 V vs RHE. (d) The calculated free energy of NO₃RR to NH₃ and NO₂⁻ on Cu(100) and Cu/Cu₂O at 0 V vs RHE ($T = 298.15$ K). The coverage of species on both Cu(100) and Cu(100)/Cu₂O(100) surfaces is 25%. The red, gray, blue, and orange balls represent oxygen, hydrogen, nitrogen, and copper atoms, respectively. (e) The reaction energies for the formation of H₂ on Cu(100) and Cu/Cu₂O. (f) Schematic illustration of potential-induced electrochemical reconstruction of Cu₂O cubes with different chemical states of Cu toward NO₃⁻ reduction to different products (NH₃ and NO₂⁻).

monitored via in situ Raman spectroscopy (Figure 3e). During the pulsed electrolysis process, the Raman characteristic peaks attributed to Cu₂O are always present in the Raman spectra, suggesting that pulsed electrolysis can protect the Cu⁺ species of the c-Cu/Cu₂O catalyst during the reduction reaction. Ex situ XRD results further show the presence of a mixed oxidation state of Cu⁰ and Cu⁺ in the c-Cu/Cu₂O catalyst after pulsed electrolysis (Figure S32). By quantifying NH₃ and NO₂⁻ produced under different reaction conditions, it was found that the pulsed electrolysis decreases (13.6%) the NH₃ selectivity, compared to that obtained via potentiostatic electrolysis on c-Cu/Cu₂O, along with increased selectivity (3.9%) of NO₂⁻ (Figure 3f). Additionally, the NH₃ to NO₂⁻ ratio of c-Cu/Cu₂O during potentiostatic electrolysis is 3.9, which is better than that during pulsed electrolysis (2.7; Figure S33). Consequently, the NH₃ yield rate is higher during potentiostatic than pulsed electrolysis, where the total charge across the electrodes is similar and the NO₃⁻ conversion is comparable (Figure S34). SEM images of the catalysts after pulsed electrolysis show that this selectivity difference is irrelevant to the morphological reconstruction (Figure S35). Therefore, the Cu/Cu₂O interface structure primarily facili-

tates the conversion of NO₃⁻ to NO₂⁻, while the in situ reconstructed Cu⁰ species favor the continuous protonation of NO₃⁻ for NH₃ synthesis.

In situ spectroscopic measurement and theoretical calculations were performed to understand the reaction mechanism of NO₃⁻ reduction at the molecular level. In situ attenuated total reflectance Fourier transform infrared (ATR-FTIR) spectroscopy was performed for the NO₃RR process over OD-Cu-c in the applied potential ranging from -0.1 to -1.0 V vs RHE. In the NO₃⁻-free PB electrolyte (Figure 4a), the FTIR spectra show only two positive peaks at 3311 and 1595 cm⁻¹, corresponding to O-H stretching and H-O-H bending of water molecules, respectively.⁵⁴ The increase in the intensity of these peaks as the potential becomes more negative indicates the occurrence of the HER with strong adsorption of water molecules. The characteristic IR bands during the NO₃RR were observed as early as -0.5 V vs RHE (Figure 4b). Specifically, the intensity of the negative peak at ~1350 cm⁻¹ in the FTIR spectrum, attributed to the adsorption of NO₃⁻,⁵⁵ increases negatively with an increase in cathodic potential because of the continuous consumption of NO₃⁻ on the OD-Cu-c catalyst surface. Meanwhile, the concomitant peak at

1250 cm^{-1} in the FTIR spectrum is ascribed to the stretching mode of NO_2^- , suggesting that NO_2^- is an intermediate product during the reduction process.⁵⁶ Furthermore, the characteristic peak of the bending vibration of the $-\text{NH}_2$ intermediate at 1450 cm^{-1} in the FTIR spectrum reflects NH_3 production from NO_3^- after successive hydrodeoxygenation.⁵⁹ Notably, compared to the results obtained in the blank electrolyte, the IR vibrational signals of OD-Cu-c assigned to the adsorbed water molecules are very weak over the entire range of applied potential in the NO_3^- -containing solution, probably because of the adsorption of NO_3^- on the catalytic sites and suppression of the HER by the NO_3RR . Additionally, similar fingerprints of nitrogen-containing intermediates, including NO_3^- , NO_2^- , and $-\text{NH}_2$ species, were observed in the FTIR spectrum of OD-Cu octahedrons, indicating that OD-Cu octahedrons share the same NO_3^- reduction reaction pathway as OD-Cu-c (Figure S36). In situ Raman spectra obtained at an operating potential of -0.9 V vs RHE are shown in Figures 4c and S37. The typical Raman peak of NH_3 at ~ 936 cm^{-1} gradually appears at the fifth minute on the surface of OD-Cu-c, further confirming that NH_3 is produced via the NO_3RR .⁵⁷

Based on the intermediates detected using the above spectroscopy and previous reports,⁵⁸ the reaction pathway for the synthesis of NH_3 via NO_3^- reduction on Cu and Cu/Cu₂O can be deduced. The Gibbs free energy of the reaction pathway ($^*\text{NO}_3 \rightarrow ^*\text{NO}_2 \rightarrow ^*\text{NO} \rightarrow ^*\text{N} \rightarrow ^*\text{NH} \rightarrow ^*\text{NH}_2 \rightarrow ^*\text{NH}_3$) was further calculated using DFT. The adsorption configurations of the intermediates of the NO_3RR to NH_3 on the Cu(100) and Cu/Cu₂O surfaces are shown in Figures S38–S40, respectively. The adsorption of reactants on the catalyst surface is generally a prerequisite for the reaction.⁴⁵ As shown in the Gibbs free energy diagram in Figure 4d, the adsorption of NO_3^- on Cu(100) (-0.11 eV) is spontaneous, whereas the adsorption of NO_3^- on Cu/Cu₂O (1.33 eV) is endothermic, indicating the enhanced NO_3^- adsorption of Cu(100). On Cu/Cu₂O, the hydrogenation of $^*\text{NO}$ species ($^*\text{NO} \rightarrow ^*\text{NOH}$) requires an energy of up to 0.84 eV, and therefore, this is the potential-determining step (PDS). Remarkably, the PDS of Cu(100) is the desorption of $^*\text{NH}_3$ with an energy barrier of 0.34 eV, which is lower than that of Cu/Cu₂O. Therefore, a considerably lower reaction barrier for the generation of NH_3 via the NO_3RR is obtained on Cu(100). Furthermore, the generation of NO_2^- on Cu(100) requires an energy of up to 1.34 eV, which is larger than the reaction barrier of the PDS for NH_3 , confirming that NH_3 formation is more favorable on Cu⁰ active sites. By contrast, after NO_3^- adsorption, the reaction process from NO_3^- to NO_2^- on the Cu/Cu₂O surface is thermodynamically downhill, indicating the preferential production of NO_2^- . Additionally, the ΔG for H_2 formation on the Cu(100) surface is higher than that on Cu/Cu₂O, indicating the inhibition of the HER on the Cu(100) surface (Figure 4e).³⁹ The adsorption energy of NO_3^- ($\Delta G_{^*\text{NO}_3}$) on Cu(100) and Cu(111) was also calculated (Figure S41). The results show the strong adsorption of NO_3^- on Cu(100) than Cu(111); therefore, Cu(100) exhibits more favorable NO_3RR performance than Cu(111), in agreement with the literature.^{59,60} The enhanced adsorption of NO_3^- on Cu(100) originates from its electronic structure with the d-band center closer to the Fermi level, as illustrated by the projected density of states analysis.^{14,20} These results indicate that OD-Cu and Cu/Cu₂O synthesized via the potential-induced method exhibited different product selectivities for

NO_3^- reduction, respectively (Figure 4f). OD-Cu is the genuine active phase that promotes the highly selective synthesis of NH_3 from NO_3^- . By contrast, the presence of Cu^+ favors the production of NO_2^- . Additionally, the catalytic activity of metallic Cu is related to the crystal plane due to the different electronic structures.

3. CONCLUSIONS

In summary, a Cu/Cu₂O interface model catalyst was developed for highly selective NO_3^- reduction to NH_3 , and the nature of Cu active sites and their correlation with the catalytic performance during the working process were studied. Importantly, in situ Raman spectroscopy and ex situ XRD characterizations show that Cu₂O of Cu/Cu₂O undergoes a structural transformation to the oxide-derived Cu⁰ when the applied potential changes from -0.5 to -1.0 V vs RHE. The oxide-derived Cu cube catalyst exhibits a maximum NH_3 FE of 93.9% and a productivity of 219.8 $\mu\text{mol h}^{-1} \text{cm}^{-2}$ at -0.9 V vs RHE. The well-designed pulse electrolysis experiments, in situ IR/Raman, and theoretical calculation analysis show that the reconstituted Cu⁰ is favorable for the highly selective NH_3 generation, whereas the Cu/Cu₂O interface prefers NO_2^- formation. This study provides an insight into the selective NO_3RR over Cu-based catalysts and valuable guidance for the rational optimization of efficient electrocatalysts.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acscatal.3c01315>.

Materials and methods; characterization data such as SEM images, TEM images, XRD patterns, XPS spectra, in situ Raman spectra, HAADF-STEM image, EDS patterns, UV-Vis absorption spectra, ion chromatogram spectra, ¹H NMR spectra, in situ ATR-FTIR spectra; electrochemical measurements; computational details and modeling (PDF)

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All authors have given approval to the final version of the manuscript.

Notes

The authors declare no competing financial interest.

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